

1. Two moles of an ideal gas expand isothermally from 5.00 L to 75.0 L at 350 K.
- [8]
- Calculate ΔU , ΔH , w and q if the expansion is reversible ($p_{\text{external}} = p$).
 - Calculate ΔU , ΔH , w and q if the expansion is irreversible with $p_{\text{external}} = p_{\text{final}}$.
 - Use the results from a and b to illustrate that the change in internal energy and the change in enthalpy (both state functions) depend only on the initial and final states of a system, but work and heat depend on the path taken in the process connecting the initial and final states.
2. One mole of gas is reversibly compressed from 25.0 L to 1.00 L at 300 K. Calculate the work w
- [7]
- if the gas is ideal
 - if the gas obeys the equation
- $$Z = \frac{pV_m}{RT} = 1 + \frac{B(T)}{V_m}$$
- with $B(T) = -0.116 \text{ L mol}^{-1}$.
- Use the results from a and b to show that attractive intermolecular forces make it “easier” (less work required) to compress a gas. Does this make sense? Comment briefly.
3. The heat capacity of propane at 1.00 bar is accurately represented by the quadratic equation

[5]

$$C_{pm}(T) = A_1 + A_2 T + A_3 T^2$$

with constants $A_1 = 0.5600 \text{ J K}^{-1} \text{ mol}^{-1}$

$$A_2 = 0.2756 \text{ J K}^{-2} \text{ mol}^{-1}$$

$$A_3 = -0.0001036 \text{ J K}^{-3} \text{ mol}^{-1}$$

Ten moles of propane (assumed to be an ideal gas) is reversibly cooled from 400 K to 300 K at 1.00 bar. Calculate q , w , ΔU and ΔH .

$$P = P_{ext}$$

- (Q1) a) Two moles of ideal gas expand reversibly and isothermally from 5.00 L to 75.0 L at 350 K.

isothermal ideal gas: $\Delta U = 0$

$\left(\text{proved } \left(\frac{\partial U}{\partial V} \right)_T = 0 \right)$
for ideal gases

$$\Delta H = \Delta(U + PV) = \Delta(U + nRT)$$

$$\Delta H = \Delta U + \Delta(nRT) = 0 + 0 \text{ for isothermal ideal gases}$$

const. const.

$$\Delta H = 0$$

reversible ($P = P_{ext}$) expansion:

$$w = - \int P_{ext} dV = - \int \frac{nRT}{V} dV = -nRT \int \frac{1}{V} dV$$

$$= -nRT \left(\ln V \Big|_{V_i}^{V_f} \right) = -nRT (\ln V_f - \ln V_i)$$

$$w = -nRT \ln(V_f/V_i) = -(2.00 \text{ mol}) \left(\frac{8.314 \text{ J}}{\text{K mol}} \right) (350 \text{ K}) \ln \left(\frac{75.0 \text{ L}}{5.00 \text{ L}} \right)$$

$$w = -15760 \text{ J}$$

$$\Delta U = q + w = 0$$

$$q = -w = 15760 \text{ J}$$

$$P_{ext} < P$$

$$P = P_f$$

- b) Two moles of ideal gas expand irreversibly and isothermally from 5.00 L to 75.0 L at 350 K.

$$\Delta U = 0$$

$$\Delta H = 0$$

(isothermal ideal gas)

$$w = - \int P_{ext} dV = - \int P_f dV \stackrel{(const.)}{=} -P_f \int dV = -P_f (V_f - V_i)$$

$$P_f = \frac{nRT}{V_f} = \frac{(2.00 \text{ mol}) (0.08314 \frac{\text{J}}{\text{K mol}}) (350 \text{ K})}{75.0 \text{ L}} = 0.77605 \text{ bar}$$

(Q1 b), cont.)

$$w = -P_f(V_f - V_i)$$

$$= -(0.7760 \text{ bar})(75.0 \text{ L} - 5.00 \text{ L}) \left(10^5 \frac{\text{Pa}}{\text{bar}}\right) \left(10^{-3} \frac{\text{m}^3}{\text{L}}\right)$$

$w = -5430 \text{ J}$

$q = 5430 \text{ J}$

convert $\text{L} \cdot \text{bar}$
to $\text{m}^3 \cdot \text{Pa} = \text{J}$

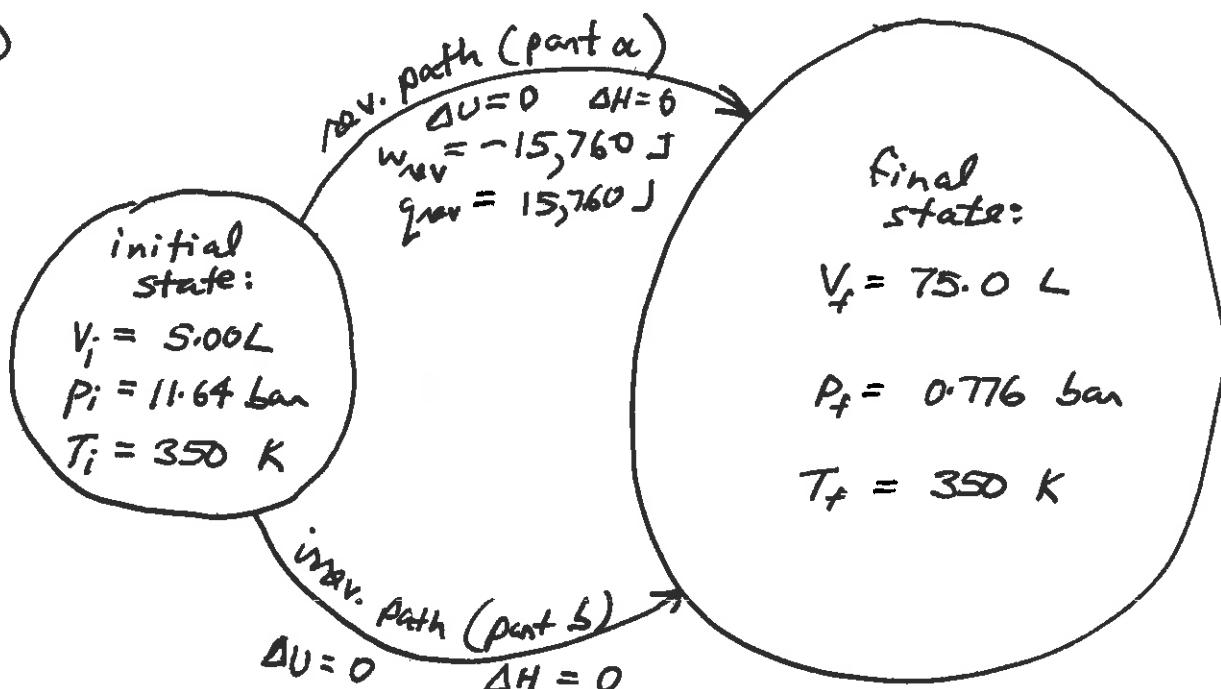
(because $\Delta U = q + w = 0$)

notice the reversibly expanding gas does more work
on the surroundings than the irreversibly expanding gas:

$$w_{\text{rev}} = -15760 \text{ J}$$

$$w_{\text{irrev}} = -5430 \text{ J}$$

c)



ΔU and ΔH are path-independent (U and H are state functions)

q and w depend on the path taken

$w_{\text{rev}} \neq w_{\text{irrev}}$
 $q_{\text{rev}} \neq q_{\text{irrev}}$

$$P_{ext} = P$$

- (Q2) a) One mole of an ideal gas is reversibly compressed from 25.0 L to 1.00 L at 300 K.

$$w = - \int P_{ext} dV = - \int pdV = - \int \frac{nRT}{V} dV = -nRT \int \frac{1}{V} dV$$

$$w = -(nRT) \ln V_f \Big|_{V_i} = -nRT (\ln V_f - \ln V_i) = -nRT \ln \left(\frac{V_f}{V_i} \right)$$

$$w = -(1.00 \text{ mol}) \left(8.314 \frac{\text{J}}{\text{Kmol}} \right) (300\text{K}) \ln \left(\frac{1.00\text{L}}{25.0\text{L}} \right)$$

$$w = 8028 \text{ J}$$

- b) One mole of a gas obeying the equation of state

$$z = \frac{PV_m}{RT} = 1 + \frac{B(T)}{V_m} \quad [B(T) = -0.116 \frac{\text{L}}{\text{mol}}]$$

is reversibly compressed ($P_{ext} = P$) from 25.0 L to 1.00 L at 300 K.

$$w = - \int P_{ext} dV = - \int pdV = - \int z \frac{RT}{V_m} dV$$

rearrange $\frac{PV_m}{RT} = \frac{pV}{nRT} = 1 + \frac{B(T)}{V_m}$

to get $P = \frac{RT}{V_m} \left(1 + \frac{B(T)}{V_m} \right) = \frac{RT}{V_m} + RTB(T) \frac{1}{V_m^2}$

(Q2 b) cont.)

$$\text{work } w = - \int p dV = - \int \left(\frac{RT}{V_m} + \frac{RT\beta(T)}{V_m^2} \right) dV$$

$$w = - \int \left(\frac{nRT}{V} + \frac{n^2 RT \beta(T)}{V^2} \right) dV$$

$$= - \int \frac{nRT}{V} dV - \int \frac{n^2 RT \beta(T)}{V^2} dV$$

$n, R, T, \beta(T)$
constant

$$= - nRT \int \frac{dV}{V} - n^2 RT \beta(T) \int \frac{dV}{V^2}$$

$$= - nRT \left(\ln V_f \right) - nRT \beta(T) \left(-\frac{1}{V} \right) \Big|_{V_i}^{V_f}$$

$$= - nRT \left(\ln \frac{V_f}{V_i} \right) - nRT \beta(T) \left[-\frac{1}{V_f} - \left(-\frac{1}{V_i} \right) \right]$$

$$= - nRT \ln \left(\frac{V_f}{V_i} \right) - nRT \beta(T) \left(\frac{1}{V_i} - \frac{1}{V_f} \right)$$

$$= -(1.00 \text{ mol}) \left(0.08314 \frac{\text{L bar}}{\text{K mol}} \right) (300 \text{ K}) \ln \left(\frac{1.00 \text{ L}}{25.0 \text{ L}} \right)$$

$$= (1.00 \text{ mol}) \left(0.08314 \frac{\text{L bar}}{\text{K mol}} \right) (300 \text{ K}) \left(-0.116 \frac{\text{L}}{\text{mol}} \right) \left(\frac{1}{25.0 \text{ L}} - \frac{1}{1.00 \text{ L}} \right)$$

$$= 80.28 \text{ L bar} - 2.78 \text{ L bar}$$

conversion factor:
 $1 \text{ L bar} = 100 \text{ J}$

$$= 77.5 \text{ L bar}$$

$$= (77.5 \text{ L bar}) \left(10^{-3} \frac{\text{m}^3}{\text{L}} \right) \left(10^5 \frac{\text{Pa}}{\text{bar}} \right)$$

w = 7750 J

(Q2 cont.)

c) ideal gas compression (part a) $w = 8028 \text{ J}$

real gas compression (part b) $w = 7750 \text{ J}$
with $B = -0.116 \text{ L mol}^{-1}$

$$\therefore z = 1 + \frac{B}{V_m} < 1 \Rightarrow \text{attractive forces dominate}$$

Less work required to compress a real gas with attractive intermolecular forces relative to an ideal gas with no intermolecular forces

makes sense: attractive forces help to pull molecules together as they are compressed

(Q3) 10.0 mol propane (assumed to be an ideal gas)
reversibly cooled from 400 K to 300 K at 1.00 bar

q ? w ? ΔH ? ΔU ?

At constant pressure (1.00 bar here) $q = \Delta H$
and $dq = dH$.

The enthalpy of the propane (treated as an ideal gas)
depends only on T .
 $(H_m = \frac{H}{n})$

At constant pressure:

$$\text{heat capacity } C_p = \frac{dH(T)}{dT} = n \frac{dH_m(T)}{dT} = n C_{pm}$$

$$dq = dH = n C_{pm} dT$$

Integrate C_{pm}
to calculate q and ΔH

(Q 3 cont.)

enthalpy change

$$\Delta H = \int_{H_i}^{H_f} dH = \int_{T_i}^{T_f} nC_{pm} dT$$

$$= n \int_{T_i}^{T_f} (A_1 + A_2 T + A_3 T^2) dT$$

$$= nA_1 \int_{T_i}^{T_f} dT + nA_2 \int_{T_i}^{T_f} T dT + nA_3 \int_{T_i}^{T_f} T^2 dT$$

$$= nA_1(T) \Big|_{T_i}^{T_f} + nA_2\left(\frac{T^2}{2}\right) \Big|_{T_i}^{T_f} + nA_3\left(\frac{T^3}{3}\right) \Big|_{T_i}^{T_f}$$

$$= nA_1(T_f - T_i) + \frac{nA_2}{2}(T_f^2 - T_i^2) + \frac{nA_3}{3}(T_f^3 - T_i^3)$$

$$\Delta H = (1.00 \text{ mol}) \left(0.5600 \frac{\text{J}}{\text{K mol}} \right) (300 - 400) \text{ K}$$
n = 1.00 mol

$$+ (1.00 \text{ mol}) \left(\frac{0.2756}{2} \frac{\text{J}}{\text{K}^2 \text{ mol}} \right) (300^2 - 400^2) \text{ K}^2$$

$$+ (1.00 \text{ mol}) \left(-\frac{0.0001036}{3} \frac{\text{J}}{\text{K}^3 \text{ mol}} \right) (300^3 - 400^3) \text{ K}^3$$

$$\Delta H = -560 \text{ J} - 96460 \text{ J} + 12770 \text{ J}$$

$\Delta H = -84,250 \text{ J} = q$

pressure p is constant (1.00 bar)

$$w = - \int P_{ext} dV = -p \int dV = -p(V_f - V_i) = -p \left(\frac{nRT_f}{P} - \frac{nRT_i}{P} \right)$$

$$w = -nR(T_f - T_i) = -(1.00 \text{ mol}) (8.314 \frac{\text{J}}{\text{K mol}}) (300 \text{ K} - 400 \text{ K})$$

$w = 8314 \text{ J}$

$$q + w = -84,250 \text{ J} + 8314 \text{ J} = \Delta U$$

$\Delta S = -75,940 \text{ J}$