

1. a) Air at 25 °C and 1.00 bar is compressed reversibly and adiabatically to 1/9 of its initial volume. In class, we showed the compressed air is *hot* (445 °C). But the compression is adiabatic: no heat flows into the air as it is compressed. So why does the air get so hot? Explain.  
 [2] b) If helium is compressed in this process, instead of air, helium gets *hotter* (1020 °C)! Why?

2. If the valve on the tank of compressed carbon dioxide in the Chem 231 lab is opened, the  
 [1] expanding gas produces a jet of solid white particles resembling snow! Explain.

3. For an ideal gas ( $V = nRT/p$ ), evaluate the following partial derivatives of the volume:

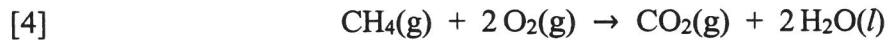
[4] a)  $\left(\frac{\partial V}{\partial T}\right)_{p,n}$       b)  $\left(\frac{\partial V}{\partial p}\right)_{T,n}$       c)  $\left[\frac{\partial}{\partial p} \left(\frac{\partial V}{\partial T}\right)_{p,n}\right]_{T,n}$       d)  $\left[\frac{\partial}{\partial T} \left(\frac{\partial V}{\partial p}\right)_{T,n}\right]_{p,n}$

This Question illustrates the useful rule  $\partial^2 f(x,y)/\partial x \partial y = \partial^2 f(x,y)/\partial y \partial x$ .

4. 5.00 moles of liquid water at its normal boiling point (100 °C, 1.00 atm) evaporates to form water vapor at the same temperature and pressure. Calculate  $q$ ,  $w$ ,  $\Delta U$  and  $\Delta H$ .

Data: Use 40.7 kJ mol<sup>-1</sup> for the enthalpy of vaporization, 0.958 g cm<sup>-3</sup> for the density of liquid water.

5. The First Law applies to chemical processes too! Calculate  $q$ ,  $w$ ,  $\Delta U$  and  $\Delta H$  for the combustion of methane at 25 °C and 1.00 bar.



Data at 25 °C, 1.00 bar:     $\Delta H_{\text{mf}}^\circ(\text{CH}_4, g) = -74.8 \text{ kJ mol}^{-1}$   
                                 $\Delta H_{\text{mf}}^\circ(\text{CO}_2, g) = -393.5 \text{ kJ mol}^{-1}$   
                                 $\Delta H_{\text{mf}}^\circ(\text{H}_2\text{O}, l) = -285.8 \text{ kJ mol}^{-1}$   
                                density  $\text{H}_2\text{O}(l) = 0.997 \text{ g cm}^{-3}$

6. 5.00 L of helium initially at 16.0 bar and 300 K expands adiabatically to 40.00 L and 0.500 bar.

- [3] a) Is the expansion reversible? Briefly justify your answer.  
 b) Calculate  $q$ ,  $w$ ,  $\Delta U$  and  $\Delta H$

7. a) The isothermal compressibility is defined as  $\kappa = -V^{-1}(\partial V/\partial p)_T$ . Why is there a minus sign?

- [2] b) In terms of the density ( $\rho$  = mass per unit volume), show  $\kappa = \rho^{-1}(\partial \rho/\partial p)_T$ .

- (Q1) a) Air (or any other gas) compressed adiabatically ( $q=0$ ) gets hot! Why? No heat is flowing into the gas.

From the First Law:  $\Delta U = q + w$ .

For an adiabatic process ( $q=0$ ):  $\Delta U_{\text{ad}} = w_{\text{ad}}$ .

During an adiabatic compression of an ideal gas, work is done on the gas ( $w>0$ ), so the energy of the gas increases:  $\Delta U_{\text{ad}} = w_{\text{ad}} > 0$ .

The energy of a gas increases with temperature.

If  $\Delta U_{\text{ad}} > 0$ , then  $\Delta T_{\text{ad}} > 0$ .

- b) For a reversible adiabatic compression:

$$dU = dq + dw \quad (\text{First Law})$$

$$dU_{\text{ad}} = dw_{\text{ad}} = -P_{\text{ext}} dV = -pdV$$

He has a smaller heat capacity than air, "easier" to warm up

for an ideal gas, the internal energy  $U$  depends only on  $T$ :

$$\text{so } dU = C_V dT = -pdV$$

$$dT = -\frac{P}{C_V} dV \quad (\text{proportional to } \frac{1}{C_V})$$

$C_V$  for He ( $\frac{3}{2}R$  per mole) is smaller than  $C_V$  for air ( $\frac{5}{2}R$  per mole)  
so the change in temperature for He is larger than  $\Delta T$  for air

(Q2)

High-pressure  $\text{CO}_2$  in the tank expands rapidly and therefore adiabatically ( $q=0$ , no time for heat flow) into the Chem 231 lab at 1.00 bar external pressure.

$\delta$  (adiabatic)

$$dU = \cancel{dq} + dw$$

$$C_V dT = -P_{\text{ext}} dV$$

$$dT = -\frac{P_{\text{ext}}}{C_V} dV$$

for the expansion of the  $\text{CO}_2$  gas,  $dV > 0$

$P_{\text{ext}} > 0$  and  $C_V > 0$ , so  $dT < 0$

The adiabatically expanding  $\text{CO}_2$  gas cools ( $dT < 0$ ), reaching temperatures below the sublimation temperature of  $\text{CO}_2$  (195 K at 1 bar)



Some  $\text{CO}_2$  freezes

The "snow" consists of solid  $\text{CO}_2$  particles aka dry ice.

[ $\text{CO}_2$  gas cooled by the adiabatic expansion freezes]

(Q3)

$$\text{a) } \left( \frac{\partial V}{\partial T} \right)_{P,n} = \left( \frac{\partial}{\partial T} \frac{nRT}{P} \right)_{P,n} = \frac{nR}{P} \left( \frac{\partial T}{\partial T} \right)_{P,n}$$

$$= \frac{nR}{P}$$

$$= \frac{V}{T}$$

(Q3 cont.)

b)  $\left(\frac{\partial V}{\partial P}\right)_{T,n} = \left(\frac{\partial}{\partial P} \frac{nRT}{P}\right)_{T,n} = nRT \left(\frac{\partial \frac{1}{P}}{\partial P}\right)_{T,n}$

$$= nRT \left(-\frac{1}{P^2}\right) = -\frac{nRT}{P^2} = -\frac{V}{P}$$

c)  $\left[\frac{\partial}{\partial P} \left(\frac{\partial V}{\partial T}\right)_{P,n}\right]_{T,n} = \left(\frac{\partial}{\partial P} \frac{nR}{P}\right)_{T,n} = nR \left(\frac{\partial \frac{1}{P}}{\partial P}\right)_{T,n}$

$$= nR \left(-\frac{1}{P^2}\right) = -\frac{nR}{P^2} = -\frac{V}{TP}$$

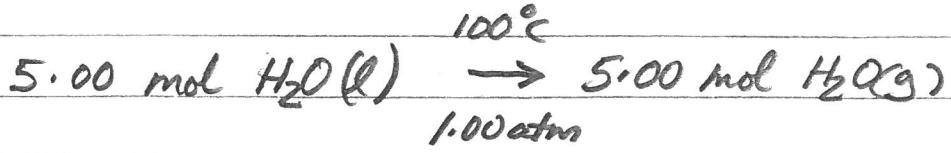
d)  $\left[\frac{\partial}{\partial T} \left(\frac{\partial V}{\partial P}\right)_{T,n}\right]_{P,n} = \left(\frac{\partial}{\partial T} -\frac{nRT}{P^2}\right)_{P,n}$

$$= -\frac{nR}{P^2} \left(\frac{\partial T}{\partial P}\right)_{P,n} = -\frac{nR}{P^2} = -\frac{V}{TP}$$

notice  $\frac{\partial^2 V}{\partial P \partial T} = \frac{\partial^2 V}{\partial T \partial P}$

$$\begin{matrix} \nearrow & \nearrow \\ c & d \end{matrix}$$

Q4



$$\Delta H = n \Delta H_{\text{vap, m}} = (5.00 \text{ mol})(40.7 \text{ kJ mol}^{-1})$$

$\Delta H = q = 203.5 \text{ kJ}$

$$\begin{aligned} w &= - \int P_{\text{ext}} dV \\ &= - \int p dV \quad (p \text{ constant}) \\ &= - p \int dV \\ &= - p \Delta V \end{aligned}$$

at constant pressure

$$\begin{aligned} q &= \Delta H \\ \text{why? } dH &= dU + pdV \\ &= dU + \cancel{pdV} \\ &= dq - pdV + pdV \\ dH_p &= dq \end{aligned}$$

$$\Delta V = n V_m(H_2O, g) - n V_m(H_2O, l)$$

$$\text{density } \rho = \frac{\text{mass}}{\text{volume}}$$

$$\text{volume} = \frac{\text{mass}}{\rho}$$

$$= n \frac{RT}{P} - n \frac{\text{molar mass}}{\text{density}}$$

$$= 5.00 \text{ mol} \left[ \frac{(0.08314 \text{ L bar K}^{-1} \text{ mol}^{-1})(373.15 \text{ K})}{1.01325 \text{ bar}} - \frac{18.01 \text{ g mol}^{-1}}{0.958 \text{ g cm}^{-3}} \right]$$

$$= 5.00 \text{ mol} \left[ 30.62 \text{ L mol}^{-1} - 18.80 \text{ cm}^3 \text{ mol}^{-1} \right]$$

$$= 5.00 \text{ mol} \left[ 30.62 \text{ L mol}^{-1} - 0.01880 \text{ L mol}^{-1} \right] \quad (\text{negligibly small})$$

$$= (5.00 \text{ mol})(30.60 \text{ L mol}^{-1}) = 153.0 \text{ L} = 0.1530 \text{ m}^3$$

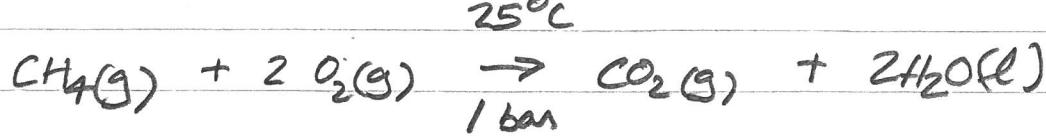
$$w = -p\Delta V = -(101325 \text{ Pa})(0.1530 \text{ m}^3)$$

$$w = -15,500 \text{ J}$$

$$\Delta U = q + w = 203.5 - 15.5$$

$$\Delta U = 188.0 \text{ kJ}$$

(Q5)



$$q = \Delta H \quad (\text{constant pressure})$$

$(1 \text{ bar} = P^{\circ}$   
standard pressure)

$$= \Delta H_f^{\circ}(\text{products}) - \Delta H_f^{\circ}(\text{reactants})$$

$$= \Delta H_{f,m}^{\circ}(\text{CO}_2, g) + 2 \Delta H_{f,m}^{\circ}(\text{H}_2\text{O}, l) - \Delta H_{f,m}^{\circ}(\text{CH}_4, g) - 2 \Delta H_{f,m}^{\circ}(\text{O}_2, g)$$

$$= [-393.5 + 2(-285.8) - (-74.8) - 2(0)] \text{ kJ}$$

$$\boxed{\Delta H = -890.3 \text{ kJ} = q}$$

$$W = - \int p_{\text{ext}} dV = - \int p dV = -p \int dV = -p \Delta V$$

$$\Delta V = V(\text{products}) - V(\text{reactants})$$

$$= V_m(\text{CO}_2, g) + 2V_m(\text{H}_2\text{O}, l) - V_m(\text{CH}_4, g) - 2V_m(\text{O}_2, g)$$

$$= \frac{RT}{P} + 2 \frac{M_{\text{H}_2\text{O}(l)}}{P_{\text{H}_2\text{O}(l)}} - \frac{RT}{P} - 2 \frac{RT}{P}$$

negligible  
volume for  
 $\text{H}_2\text{O}(l)$

$$= -\frac{2RT}{P} + 2 \frac{18.01 \text{ g mol}^{-1}}{0.997 \text{ g cm}^{-3}} = -\frac{2(0.08314)(298.15)}{1.00} \text{ L} + 36.0 \text{ cm}^3$$

$$= -49.58 \text{ L} + 0.036 \text{ L} = -49.54 \text{ L} = -0.04954 \text{ m}^3$$

$$W = -p \Delta V = -(1.00 \text{ bar})(-49.54 \text{ L}) = 49.54 \text{ L bar}$$

$$w = (49.54 \text{ L bar}) \left( \frac{100 \text{ J}}{1 \text{ bar}} \right) = \boxed{4954 \text{ J} = w}$$

$$\Delta U = q + w = -890.3 \text{ kJ} + 4.954 \text{ kJ} = \boxed{-885.3 \text{ kJ} = \Delta U}$$

(Q6)

a) for helium:  $C_{Vm} = \frac{3}{2} R$

$\left( \frac{1}{2} R \text{ for kinetic energy in the } x, y, z \text{ directions} \right)$

$$C_{Pm} = C_{Vm} + R \text{ (ideal gas)}$$

$$= \frac{5}{2} R$$

$$\gamma = \frac{C_{Pm}}{C_{Vm}} = \frac{\frac{5}{2} R}{\frac{3}{2} R} = \frac{5}{3}$$

If the adiabatic expansion is reversible, then  $P_i V_i^\gamma = P_f V_f^\gamma$

$$P_i V_i^\gamma = (16.0 \text{ bar}) (5.00 L)^{5/3} = 233.92 \text{ bar } L^{5/3}$$

$$P_f V_f^\gamma = (0.500 \text{ bar}) (40.00 L)^{5/3} = 233.92 \text{ bar } L^{5/3}$$

$P_i V_i^\gamma = P_f V_f^\gamma$  so the expansion is reversible

b)

$$n = \frac{P_i V_i}{R T_i} = \frac{P_f V_f}{R T_f} \quad T_f = \frac{P_f V_f}{P_i V_i} T_i$$

$$T_f = \frac{(0.500 \text{ bar})(40.0 L)}{(16.0 \text{ bar})(5.00 L)} 300 K = 75 K$$

$$\Delta U = W = n C_{Vm} (T_f - T_i)$$

$$= \frac{3}{2} (3.21 \text{ mol}) \left( \frac{8.314 \text{ J}}{\text{K mol}} \right) (75 - 300) \text{ K}$$

$\boxed{\Delta U = W = -9010 \text{ J}}$

$$\left( \begin{array}{l} n = \frac{16.0 \cdot 5.00}{0.08314 \cdot 300} \\ n = 3.21 \text{ mol} \end{array} \right)$$

$$\Delta H = n C_{Pm} \Delta T = n \frac{5}{2} R \Delta T$$

$\boxed{\Delta H = -15,020 \text{ J}}$

recall:  $C_{Vm} = C_{Vm} + R$  (ideal gas)

(Q7)

a)  $\left(\frac{\partial V}{\partial P}\right)_T$  is always negative

(systems shrink in volume if the pressure is increased)

defining  $\kappa$  as  $-\frac{1}{V} \left(\frac{\partial V}{\partial P}\right)_T$  is convenient

because  $\kappa$  is always positive (don't have to include a minus sign for  $\kappa$  values)

b) volume  $V = \frac{\text{mass}}{\text{density}} = \frac{m}{\rho}$

$$\begin{aligned} \kappa &= -\frac{1}{V} \left(\frac{\partial V}{\partial P}\right)_T = -\frac{1}{\frac{m}{\rho}} \left(\frac{\partial}{\partial P} \frac{m}{\rho}\right)_T = -\frac{m}{\frac{m}{\rho}} \left(\frac{\partial \frac{1}{\rho}}{\partial P}\right)_T \\ &= -\rho \left(-\frac{1}{\rho^2}\right) \left(\frac{\partial \rho}{\partial P}\right)_T = \frac{1}{\rho} \left(\frac{\partial \rho}{\partial P}\right)_T \end{aligned}$$