

- please answer all 5 questions in the spaces provided
- you have two hours to write this test
- a calculator and the equation sheet provided may be used
- all questions are of equal value
- no books or notes are allowed,
- no marks for unreadable answers

1. a) A tank is filled with compressed natural gas (assumed to be pure methane, MW 16.0 g mol<sup>-1</sup>) at 20 °C and a density of 225 grams per liter.  $T = (20 + 273)K = 293 K$

- i) Calculate the pressure in the tank using the ideal gas equation.

$$\text{molar volume } V_m = \frac{1.00 \text{ L}}{(225 \text{ g}) / (16.0 \text{ g mol}^{-1})} = 0.07111 \text{ L mol}^{-1}$$

$$P = \frac{nRT}{V} = \frac{RT}{V/n} = \frac{RT}{V_m} = \frac{(0.08314 \text{ L bar K}^{-1} \text{ mol}^{-1})(293 \text{ K})}{0.07111 \text{ L mol}^{-1}}$$

$$P = 343 \text{ bar}$$

- ii) Calculate the pressure in the tank using the van der Waals equation.

$$(a = 2.28 \text{ bar L}^2 \text{ mol}^{-2} \text{ and } b = 0.0427 \text{ L mol}^{-1})$$

$$P = \frac{RT}{V_m - b} - \frac{a}{V_m^2}$$

$$= \frac{(0.08314 \text{ L bar K}^{-1} \text{ mol}^{-1})(293 \text{ K})}{(0.07111 - 0.0427) \text{ L mol}^{-1}} - \frac{2.28 \text{ bar L}^2 \text{ mol}^{-2}}{(0.07111 \text{ L mol}^{-1})^2}$$

$$= 858.4 \text{ bar} - 450.9 \text{ bar}$$

$$P = 408 \text{ bar}$$

- iii) Do attractive intermolecular forces dominate repulsive forces? Justify your answer.

No

repulsive methane intermolecular forces dominate

$$P_{\text{real}} > P_{\text{ideal}} \\ (\text{part ii}) \quad (\text{part i})$$

- b) Large amounts of methane are transported in liquid form, not as the compressed gas. Why?

Liquefied natural gas is at atmospheric pressure. Does not require thick-wall high pressure tanks or pipelines. Can be shipped economically worldwide.

$$P_i V_i = P_f V_f = nRT \Rightarrow \frac{V_f}{V_i} = \frac{P_i}{P_f}$$

2. 1.00 mole of an ideal gas expands isothermally from 8.00 bar to 2.00 bar at 300 K:

a) Calculate  $w$ ,  $q$ ,  $\Delta U$  and  $\Delta H$  if the expansion is reversible.

$$\Delta U = 0 \quad \text{and} \quad \Delta H = 0$$

$P_{\text{ext}} = P$   
(isothermal ideal gas)  
(isothermal)

$$w = - \int P_{\text{ext}} dV = - \int P dV = - \int \frac{nRT}{V} dV$$

$$w = - nRT \int_{V_i}^{V_f} \frac{1}{V} dV = - nRT \ln\left(\frac{V_f}{V_i}\right) = - nRT \ln\left(\frac{P_i}{P_f}\right)$$

$$w = - (1.00 \text{ mol}) (8.314 \text{ J K}^{-1} \text{ mol}^{-1}) (300 \text{ K}) \ln\left(\frac{8.00 \text{ bar}}{2.00 \text{ bar}}\right)$$

$$w = -3460 \text{ J}$$


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$$q = 3460 \text{ J}$$

$$\begin{cases} \Delta U = q + w \\ 0 = q + w \quad \Rightarrow \quad q = -w \end{cases}$$

b) Calculate  $w$ ,  $q$ ,  $\Delta U$  and  $\Delta H$  if the expansion is irreversible with  $p_{\text{ext}} = 2.00$  bar.

$$\Delta U = 0 \quad \text{and} \quad \Delta H = 0$$

$$w = - \int P_{\text{ext}} dV = - \int_{V_i}^{V_f} P_f dV = - P_f \int_{V_i}^{V_f} dV = - P_f (V_f - V_i)$$

$$w = - P_f V_f + P_f V_i = - nRT + \frac{P_f}{P_i} P_i V_i = - nRT + \frac{P_f}{P_i} nRT$$

$$w = nRT \left(\frac{P_f}{P_i} - 1\right) = (1.00 \text{ mol}) (8.314 \text{ J K}^{-1} \text{ mol}^{-1}) (300 \text{ K}) \left(\frac{2.00 \text{ bar}}{8.00 \text{ bar}} - 1\right)$$

$$w = -1870 \text{ J} \quad q = -w = 1870 \text{ J}$$

$$\left( \begin{array}{l} \text{or, use } V_i = RT/P_i = 3.118 \text{ L} \\ V_f = RT/P_f = 12.471 \text{ L} \end{array} \right. \quad \left. \begin{array}{l} w = -P_f (V_f - V_i) \\ = -2.00 (12.471 - 3.118) \text{ L bar} \\ w = -1870 \text{ J} \end{array} \right)$$

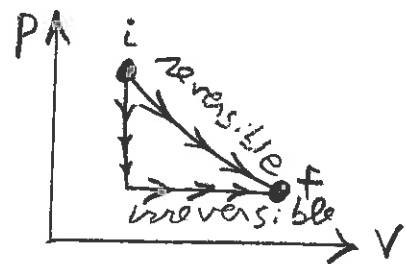
c) Use the answers to a and b to illustrate that  $U$  and  $H$  are state functions, but  $q$  and  $w$  are path-dependent.

$$\Delta U(\text{rev. path}) = \Delta U(\text{irrev. path})$$

$$\Delta H(\text{ " }) = \Delta H(\text{ " })$$

$$w(\text{rev. path}) \neq w(\text{irrev. path})$$

$$q(\text{ " }) \neq q(\text{ " })$$



3. a) Use the thermodynamic equation of state to prove  $(\partial U/\partial V)_T = 0$  for ideal gases.

ideal gas:  $p = \frac{nRT}{V}$  (hint  $(\frac{\partial U}{\partial V})_T = T(\frac{\partial p}{\partial T})_V - p$ )

$$\left(\frac{\partial U}{\partial V}\right)_T = T\left(\frac{\partial p}{\partial T}\right)_V - p = T\left(\frac{\partial \frac{nRT}{V}}{\partial T}\right)_V - p = T \frac{nR}{V} \left(\frac{\partial T}{\partial T}\right)_V - p$$

$$= \frac{TnR}{V}(1) - p = \frac{nRT}{V} - \frac{nRT}{V} = 0$$

b) Show  $(\partial C_V/\partial V)_T = 0$  for ideal gases.

(hint  $C_V = (\partial U/\partial T)_V$ )

$$\left(\frac{\partial C_V}{\partial V}\right)_T = \left[\frac{\partial}{\partial V} \left(\frac{\partial U}{\partial T}\right)_V\right]_T = \left[\frac{\partial}{\partial T} \left(\frac{\partial U}{\partial V}\right)_T\right]_V$$

order of differentiation "doesn't matter"

$$= \left[\frac{\partial}{\partial T} 0\right]_V = 0 \quad \left[\left(\frac{\partial U}{\partial V}\right)_T = 0 \text{ from part a)}\right]$$

c) Show  $dq = C_V dT + p dV$  for reversible processes for ideal gases. (hint  $dU = dq + dw$ )

ideal gas ( $U$  depends only on  $T$ ):  $dU = C_V dT$

reversible expansion/compression:  $dw = -p dV$   
( $P = P_{ext}$ )

First Law:  $dU = dq + dw$

Ideal Gas:  $C_V dT = dq - p dV$

"":  $dq = C_V dT + p dV$

d) Use  $dq = C_V dT + p dV$  to prove the function  $q(T, V)$  does not exist for ideal gases.

$$dq = g(T, V) dT + h(T, V) dV$$

$g = C_V$   
 $h = p$

$g(T, V)$  exists if  $\left(\frac{\partial g}{\partial V}\right)_T \stackrel{?}{=} \left(\frac{\partial h}{\partial T}\right)_V$

$$\left(\frac{\partial g}{\partial V}\right)_T = \left(\frac{\partial C_V}{\partial V}\right)_T = 0 \text{ (part b)}$$

$$\left(\frac{\partial h}{\partial T}\right)_V = \left(\frac{\partial p}{\partial T}\right)_V = \left(\frac{\partial \left(\frac{nRT}{V}\right)}{\partial T}\right)_V = \frac{nR}{V} \left(\frac{\partial T}{\partial T}\right)_V = \frac{nR}{V} \neq 0$$

$q(T, V)$  does not exist

4. a) 5.00 L of liquid water initially at 1.00 bar and 25.0 °C is compressed isothermally. The final pressure is 100.0 bar. For this process:

i) calculate the volume change (use  $\kappa = 4.59 \times 10^{-5} \text{ bar}^{-1}$ , assumed to be constant)

$$\kappa = -\frac{1}{V} \left( \frac{\partial V}{\partial P} \right)_T \Rightarrow -\kappa dP = \frac{dV}{V} \Rightarrow -\int \kappa dP = \int \frac{dV}{V}$$

$$-\kappa(P_f - P_i) = \ln \frac{V_f}{V_i} \quad e^{-\kappa(P_f - P_i)} = \frac{V_f}{V_i}$$

$$V_f = V_i e^{-\kappa(P_f - P_i)}$$

$$V_f = (5.00 \text{ L}) e^{-(4.59 \times 10^{-5} \text{ bar}^{-1})(100 - 1) \text{ bar}} = (5.00 \text{ L}) e^{-0.00454}$$

$$V_f = (5.00 \text{ L})(0.99547) = 4.977 \text{ L}$$

$$\Delta V = V_f - V_i = (4.977 - 5.00) \text{ L} = \boxed{-0.023 \text{ L}}$$

ii) explain why is unnecessary to specify if the compression is reversible ( $p_{\text{ext}} = p$ ) or irreversible ( $p_{\text{ext}} = 100.0 \text{ bar}$ ) in order to calculate the volume change

The volume of liquid water is a function of the state variables  $T, P$

$$\Delta V = V(T_f, P_f) - V(T_i, P_i)$$

is therefore path independent

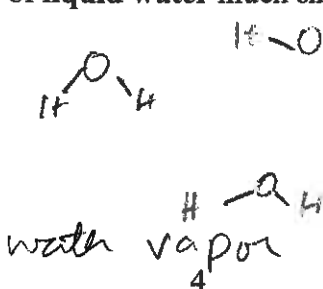
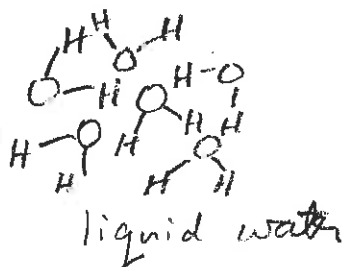
b) Calculate  $\kappa$  for water vapor (assumed to be an ideal gas) at 1.00 bar and 25 °C.

ideal gas

$$\kappa = \frac{1}{P} = \frac{1}{1.00 \text{ bar}}$$

$$\boxed{\kappa = 1.00 \text{ bar}^{-1}}$$

c) Why is the compressibility of liquid water much smaller than that of water vapor?



liquid water molecules are tightly packed together compared to vapor molecules: (no "free" volume to compress into)

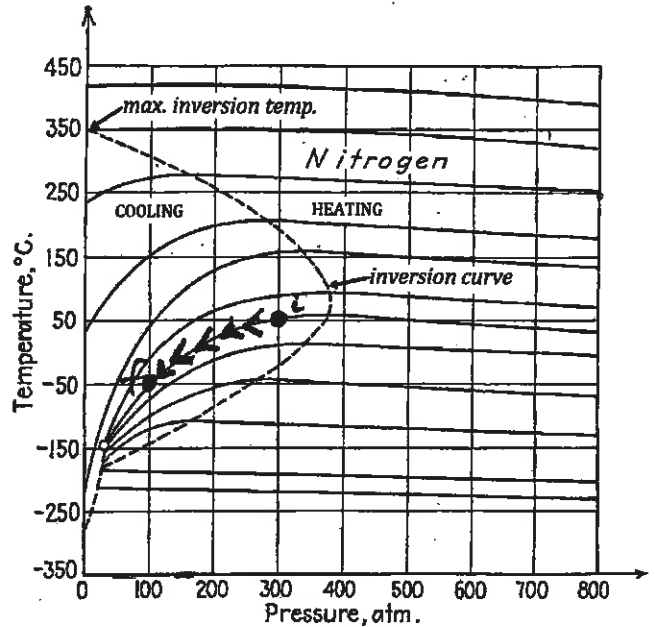
5. a) Nitrogen gas initially at 300 atm and 50 °C undergoes a Joule-Thomson expansion.

The final pressure is 100 atm.

Use the graph provided to estimate the final temperature.

read from graph =

-50 °C



- b) Suggest why the Joule-Thomson expansion of an ideal gas is also an isothermal expansion.

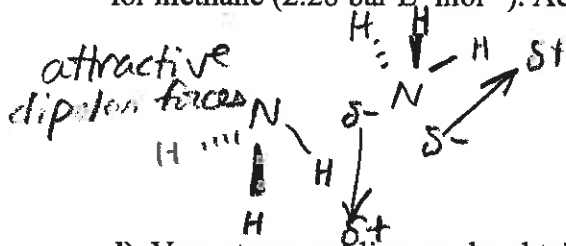
JT expansions are "isenthalpic" (constant H)

For an ideal gas, H depends only on T.

If H is constant, then so is T.

- c) Ammonia and methane molecules have the same number of electrons (10) and therefore might be expected to have similar intermolecular dispersion forces.

But the van der Waals  $a$  parameter for ammonia ( $4.24 \text{ bar L}^2 \text{ mol}^{-2}$ ) is significantly larger than  $a$  for methane ( $2.28 \text{ bar L}^2 \text{ mol}^{-2}$ ). Account for this apparent discrepancy.



$\text{NH}_3$  molecules have permanent electric dipoles,  $\text{CH}_4$  molecules are nonpolar.

electric dipole interactions increase  $a$  for  $\text{NH}_3$

- d) Very strong cooling can be obtained by adiabatically expanding ideal gases (Problem Set #3). But when an ideal gas expands into a vacuum ( $p_{\text{ext}} = 0$ ), show there is no temperature change!

$$dU = dq + dw \quad \text{First Law}$$

$$C_v dT = dq - p_{\text{ext}} dV$$

(Ideal gas,  $U$  depends on  $T$  only)  
 $dU = C_v dT$

$$C_v dT = 0 - p_{\text{ext}} dV \quad (\text{adiabatic } q=0)$$

$$C_v dT = 0 - 0 \quad (p_{\text{ext}} = 0)$$

$$dT = 0$$

$\Delta U = q = w = 0!$

Q1  
Q2  
Q3  
Q4  
Q5