

- please answer all **5 questions** in the spaces provided
- you have **two hours** to write this test
- a calculator and the equation sheets provided may be used

- all questions are of equal value
- no books or notes are allowed
- no marks for unreadable answers

1. a) Carbon monoxide is oxidized at 25°C and 1.00 bar: $\text{CO(g)} + \frac{1}{2}\text{O}_2\text{(g)} = \text{CO}_2\text{(g)}$

 $\cancel{P \text{ constant}}$ Calculate q , w , ΔU and ΔH .Data at 25°C

$$\begin{aligned} w &= - \int_{V_i}^{V_f} P_{\text{ext}} dV = -P \int_{V_i}^{V_f} dV \\ &= -P \Delta V = -P(V_{\text{mCO}_2} - V_{\text{mCO}} - \frac{1}{2}V_{\text{mO}_2}) \\ w &= -P\left(\frac{RT}{P} - \frac{RT}{P} - \frac{1}{2}\frac{RT}{P}\right) = \frac{RT}{2} = \frac{(8.314 \text{ J K}^{-1}\text{ mol}^{-1})(298.15 \text{ K})}{2} \end{aligned}$$

$$w = 1240 \text{ J}$$

$$\begin{aligned} \text{heat } q &= \Delta H = \Delta H_{\text{fm}}^{\circ}(\text{CO}_2, \text{g}) - \Delta H_{\text{fm}}^{\circ}(\text{CO}, \text{g}) - \frac{1}{2} \cancel{\Delta H_{\text{fm}}^{\circ}(\text{O}_2, \text{g})} \\ (\cancel{P \text{ constant}}) &= -393.509 - (-110.525) = -282.984 \text{ kJ mol}^{-1} \end{aligned}$$

$$\begin{aligned} \text{internal energy } \Delta U &= q + w = -282.984 \text{ kJ mol}^{-1} + 1.240 \text{ kJ mol}^{-1} \\ \Delta U &= -281.744 \text{ kJ mol}^{-1} \end{aligned}$$

- b) Calculate the adiabatic flame temperature if CO(g) initially at 25°C is burned in oxygen.

$$\begin{aligned} T_f &= T_i - \frac{\Delta H(T_i)}{C_p(\text{products})} = T_i - \frac{\Delta H_R^{\circ}}{C_{pm}(\text{CO}_2, \text{g})} \\ &= 298.15 \text{ K} - \frac{-282.984 \text{ J mol}^{-1}}{37.11 \text{ J K}^{-1} \text{ mol}^{-1}} \\ &= 298.15 \text{ K} + 7625 \text{ K} \end{aligned}$$

$$T_f = 7920 \text{ K}$$

- c) The flame produced by burning CO(g) in oxygen is significantly hotter than the flame produced by burning CO(g) in air. Why? Explain briefly.

In air, N_2 increases $C_p(\text{products})$:

air: about 4 mol N_2 per mol O_2



$$T_{f(\text{air})} = T_i - \frac{\Delta H_R^{\circ}}{C_{pm}(\text{CO}_2) + 2C_{pm}(\text{N}_2)} < T_f(\text{in pure O}_2)$$

Carnot cycle:



2. a) Analysis of the Carnot cycle for reversible heat engines shows $\frac{q_H}{T_H} + \frac{q_C}{T_C} = 0$. How did this result lead to the discovery of the entropy?

This result, generalized to $\oint \frac{dq_{rev}}{T} = 0$, suggested that $\frac{dq_{rev}}{T}$ is the differential of a new state function T (Why? Because $\oint f_i^i = f_i - f_i = 0$ for state functions)

- b) For a Carnot heat engine: $q_H + q_C + w = 0$. Why?

$$\text{For one cycle } \oint dU = U_i - U_i = q + w \\ = q_H + q_C + w$$

- c) A heat engine absorbs 5.00 MJ at $T_H = 500$ K and rejects 3.50 MJ heat at $T_C = 300$ K.

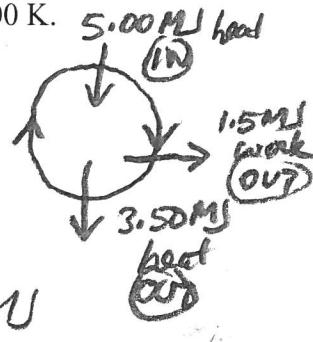
- i) Calculate the work done on the surroundings.

$$q_H = 5.00 \text{ MJ} \quad q_C = -3.50 \text{ MJ}$$

$$0 = q_H + q_C + w$$

$$-w = q_H + q_C = 5.00 \text{ MJ} - 3.50 \text{ MJ} \\ = 1.50 \text{ MJ}$$

work done on surroundings



- ii) Is the engine operating reversibly? Justify your answer.

$$\text{max efficiency (if reversible)} = 1 - \frac{T_C}{T_H} = 1 - \frac{300K}{500K} = 0.400_{\text{rev}}$$

$$\text{actual efficiency} = \frac{-w}{q_H} = \frac{1.50 \text{ MJ}}{5.00 \text{ MJ}} = \boxed{\frac{\epsilon}{0.300}} < 0.400_{\text{rev}}$$

NOT REVERSIBLE

- d) Give two practical applications of heat pumps.

air conditioning
refrigeration

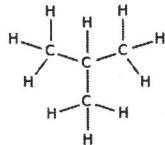
- e) 1.0 MJ of electrical work is used to run a Carnot engine in reverse. If $T_C = 290$ and $T_H = 300$ K, calculate the maximum amount of heat pumped into the reservoir at $T_H = 300$ K.

work done on the engine to pump heat (nonspontaneously)
from 290 K to 300 K: $w = +1.0 \text{ MJ}$

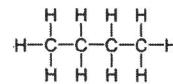
$$-\frac{w}{q_H} = 1 - \frac{T_C}{T_H} \quad -\frac{1.0 \text{ MJ}}{q_H} = 1 - \frac{290 \text{ K}}{300 \text{ K}} = 0.0333$$

$$q_H = \frac{-1.0 \text{ MJ}}{0.0333} = \boxed{-30 \text{ MJ}}$$

3. Butane is found in two common forms:



and



Data at 25 °C

iso-butane

n-butane

$$\Delta H_{fm}^{\circ}(\text{iso-butane, g}) = -134.52 \text{ kJ mol}^{-1}$$

$$\Delta H_{fm}^{\circ}(\text{n-butane, g}) = -126.15 \text{ kJ mol}^{-1}$$

$$S_m^{\circ}(\text{iso-butane, g}) = 294.75 \text{ J K}^{-1} \text{ mol}^{-1}$$

$$S_m^{\circ}(\text{n-butane, g}) = 310.23 \text{ J K}^{-1} \text{ mol}^{-1}$$

- a) Direct measurement of the enthalpies of formation of *iso*-butane and *n*-butane is very difficult. Why?



Big Problems: The reactions are very slow (nonexistent) at 25 °C and there are many side reactions.

- b) Explain how the enthalpies of formation of *iso*-butane and *n*-butane can be calculated from measured enthalpies of combustion.



$$\text{measure } \Delta H_c = 4\Delta H_{fm}^{\circ}(\text{CO}_2) + 5\Delta H_{fm}^{\circ}(\text{H}_2\text{O}) - \Delta H_{fm}^{\circ}(\text{C}_4\text{H}_{10})$$

$$\text{calculate } \Delta H_{fm}^{\circ}(\text{C}_4\text{H}_{10}) = 4\Delta H_{fm}^{\circ}(\text{CO}_2) + 5\Delta H_{fm}^{\circ}(\text{H}_2\text{O}) - \Delta H_c$$

- c) $S_m^{\circ}(\text{iso-butane, g})$ and $S_m^{\circ}(\text{n-butane, g})$ are absolute entropies, not entropies of formation. How are absolute entropies measured?

$$S_m^{\circ}(\text{C}_4\text{H}_{10}) = \int_0^T \frac{C_p^{\circ}}{T} dT + \sum_i \frac{\Delta H_{im}^{\circ}}{T_i} \quad \begin{array}{l} \text{for} \\ \text{s} \rightarrow l \\ l \rightarrow g \\ \text{phase} \\ \text{changes} \end{array}$$

at temperature T

- c) Calculate ΔS_R° for the reaction $\text{iso-butane(g)} \rightarrow \text{n-butane(g)}$ at 25 °C. ΔS_R° for the reaction is positive at 25 °C. Does this mean the reaction is spontaneous? Explain.

$$\Delta S_R^{\circ} = S_m^{\circ}(\text{n-butane}) - S_m^{\circ}(\text{iso-butane})$$

$$= (310.23 - 294.75) \text{ J K}^{-1} \text{ mol}^{-1} = 15.48 \text{ J K}^{-1} \text{ mol}^{-1}$$

ΔS_R° alone can't be used to decide spontaneity system not isolated

- d) To decide if the reaction $\text{iso-butane(g)} \rightarrow \text{n-butane(g)}$ is spontaneous, why not just buy some *iso*-butane and see if it reacts to form *n*-butane?

The reaction is very slow (immeasurably slow)

$$(\Delta H_R^{\circ} = 8370 \text{ J})$$

- e) An organic chemist argues that *n*-butane has less steric hindrance and therefore more stable than *iso*-butane. Is this correct? Use thermodynamics to decide which isomer is more stable at 25 °C.

at 25 °C, 1 bar $\Delta G_{TP} < 0$ if spontaneous

$$\text{Here: } \Delta G_R^{\circ} = \Sigma (\text{H} - TS)_R^{\circ} = \Delta H_R^{\circ} - T\Delta S_R^{\circ}$$

$$= \Delta H_{fm}^{\circ}(\text{n-but}) - \Delta H_{fm}^{\circ}(\text{iso-but}) - T\Delta S_R^{\circ}$$

$$= -126.15 - (-134.52) - (298.15)(15.48) = +3755 \text{ J}$$

$\text{iso} \rightarrow n$
 $\Delta G^{\circ} > 0$
iso more stable

not spont.

4. a) The equation

$$[5] \quad dU = \left(\frac{\partial U}{\partial T}\right)_V dT + \left(\frac{\partial U}{\partial V}\right)_T dV \quad (4.1)$$

is mathematically correct, but not very convenient for calculating energy changes. Explain.

how are $\left(\frac{\partial U}{\partial T}\right)_V$ and $\left(\frac{\partial U}{\partial V}\right)_T$ calculated?

b) Show $\left(\frac{\partial U}{\partial T}\right)_V = C_V$

$$dU = dq - P_{ext} dV \quad \text{at constant volume } dU_V = dq_V$$

$$C_V = \frac{dq_V}{dT} = \frac{dU_V}{dT} = \left(\frac{\partial U}{\partial T}\right)_V \quad \text{or: } dU = TdS - pdV \quad \div dT_V$$

$$\left(\frac{\partial U}{\partial T}\right)_V = T \left(\frac{\partial S}{\partial T}\right)_V \quad TdS = dq_{\text{non}}$$

c) Show $\left(\frac{\partial U}{\partial V}\right)_T = T \left(\frac{\partial p}{\partial T}\right)_V - p$ (hint: use $dU = TdS - pdV$ and a Maxwell relation)

$$dV = TdS - pdV \quad (\div dV_T)$$

$$\begin{aligned} \left(\frac{\partial U}{\partial V}\right)_T &= T \left(\frac{\partial S}{\partial V}\right)_T - p \\ &= T \left(\frac{\partial P}{\partial T}\right)_V - p \end{aligned}$$

d) Combining a, b and c gives

$$dU = C_V dT + \left[T \left(\frac{\partial p}{\partial T} \right)_V - p \right] dV \quad (4.2)$$

Equation (4.2) is more convenient for calculating internal energy changes than equation (4.1). Why?

$$C_V, T, \left(\frac{\partial P}{\partial T}\right)_V = \frac{\beta}{k}, P \Rightarrow \text{all measurable or can be calculated from equations of state}$$

e) Use equation (4.2) to show $dU = C_V dT$ for an ideal gas.

$$P = \frac{nRT}{V}$$

$$dU = C_V dT + \left[T \left(\frac{\partial P}{\partial T} \right)_V - P \right] dV = C_V dT + \left[T \left(\frac{\partial \frac{nRT}{V}}{\partial T} \right)_V - P \right] dV$$

$$dU = C_V dT + \left[T \frac{nR}{V} \left(\frac{\partial T}{\partial T} \right)_V - P \right] dV = C_V dT + \left[\cancel{\frac{nRT}{V}} - P \right] dV$$

$$dU = C_V dT$$

5. The "water gas shift reaction" $\text{CO(g)} + \text{H}_2\text{O(g)} = \text{CO}_2\text{(g)} + \text{H}_2\text{(g)}$ is used to produce hydrogen and carbon dioxide from carbon monoxide and steam at 1000 K.

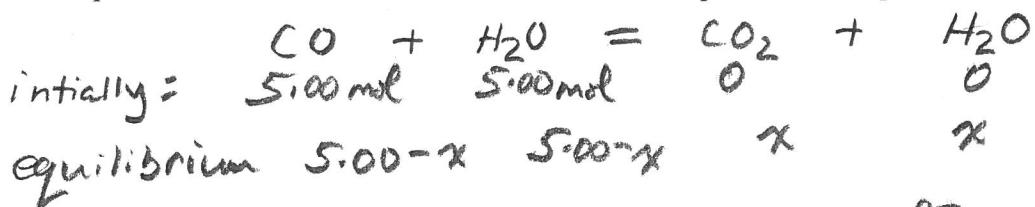
Data at 1000 K

$\Delta G_{\text{fm}}^{\circ}(\text{CO}_2, \text{g}) = -395.866 \text{ kJ mol}^{-1}$	$\Delta H_{\text{fm}}^{\circ}(\text{CO}_2, \text{g}) = -394.623 \text{ kJ mol}^{-1}$
$\Delta G_{\text{fm}}^{\circ}(\text{CO}, \text{g}) = -200.275 \text{ kJ mol}^{-1}$	$\Delta H_{\text{fm}}^{\circ}(\text{CO}, \text{g}) = -111.983 \text{ kJ mol}^{-1}$
$\Delta G_{\text{fm}}^{\circ}(\text{H}_2\text{O}, \text{g}) = -192.590 \text{ kJ mol}^{-1}$	$\Delta H_{\text{fm}}^{\circ}(\text{H}_2\text{O}, \text{g}) = -247.867 \text{ kJ mol}^{-1}$

- a) At 1000 K, show the equilibrium constant for the reaction is $K = 1.43$.

$$\begin{aligned}\Delta G_R^{\circ} &= \Delta G_{\text{fm}}^{\circ}(\text{CO}_2, \text{g}) + \Delta G_{\text{fm}}^{\circ}(\text{H}_2, \text{g}) - \Delta G_{\text{fm}}^{\circ}(\text{CO}, \text{g}) - \Delta G_{\text{fm}}^{\circ}(\text{H}_2\text{O}, \text{g}) \\ &= -395.866 + 0 - (-200.275) - (-192.590) = -3,001 \text{ J mol}^{-1} \\ K &= \exp\left(-\frac{\Delta G_R^{\circ}}{RT}\right) = \exp\left(-\frac{-3001}{8.314(1000)}\right) = e^{0.3610} = 1.434\end{aligned}$$

- b) A mixture containing 5.00 mol CO(g) and 5.00 mol H₂O(g) is heated to 1000 K at 1.00 bar total pressure. Calculate the number of moles of H₂ produced at equilibrium.



$$K = 1.43 = \frac{P_{\text{CO}_2} P_{\text{H}_2}}{P_{\text{CO}} P_{\text{H}_2\text{O}}} = \frac{\frac{n_{\text{CO}_2} RT}{V} \frac{n_{\text{H}_2} RT}{V}}{\frac{n_{\text{CO}} RT}{V} \frac{n_{\text{H}_2\text{O}} RT}{V}} = \frac{n_{\text{CO}_2} n_{\text{H}_2}}{n_{\text{CO}} n_{\text{H}_2\text{O}}}$$

$$K = \frac{x x}{(5.00-x)(5.00-x)}$$

$$\sqrt{K} = \frac{x}{5.00-x}$$

$$x = \frac{\sqrt{K}}{1+\sqrt{K}} 5.00 \text{ mol} = \boxed{2.72 \text{ mol H}_2}$$

- c) For a higher yield of H₂, should the temperature be increased? Justify your answer.

$$\begin{aligned}\Delta H_R^{\circ} &= \Delta H_{\text{fm}}^{\circ}(\text{CO}_2, \text{g}) + \Delta H_{\text{fm}}^{\circ}(\text{H}_2, \text{g}) - \Delta H_{\text{fm}}^{\circ}(\text{CO}, \text{g}) - \Delta H_{\text{fm}}^{\circ}(\text{H}_2\text{O}, \text{g}) \\ &= -394.623 + 0 - (-111.983) - (-247.867)\end{aligned}$$

$$\Delta H_R^{\circ} = -34.823 \quad \text{exothermic} \quad \left(\frac{d \ln K}{dT} = \frac{\Delta H_R^{\circ}}{RT^2} < 0 \right)$$

should decrease T for higher yield

- d) For a higher yield of H₂, should the pressure be increased? Justify your answer.

$$\text{H}_2 \text{ yield} = \frac{\sqrt{K}}{1+\sqrt{K}}$$

pressure has no effect on yield

(assuming ideal gas behavior)

NO