

- please answer all **4 questions** in the spaces provided
- this is a **50-minute test**
- a calculator and the equation sheets provided may be used

- all questions are of equal value
- no books or notes are allowed
- no marks for unreadable answers

1. a)  $P_{\text{ext}} = P$   
75.0 L of helium (assumed to be an ideal gas) at 300 K and 2.00 bar is compressed isothermally and reversibly to a final pressure of 6.00 bar. Calculate  $q$ ,  $w$ ,  $\Delta U$  and  $\Delta S$ . Hint:  $n = p_i V_i / RT = \text{constant}$

$$\Delta U = 0 \quad (\text{isothermal ideal gas})$$

$$\left(\frac{V_f}{V_i} = \frac{P_i}{P_f}\right)$$

$$\text{moles of gas } n = \frac{P_i V_i}{RT} = \frac{(2.00 \text{ bar})(75.0 \text{ L})}{(0.08314 \text{ L bar K}^{-1} \text{ mol}^{-1})(300 \text{ K})} = 6.014 \text{ mol}$$

$$w = -\int P_{\text{ext}} dV = -\int P dV = -nRT \int \frac{1}{V} dV = -nRT \ln\left(\frac{V_f}{V_i}\right)$$

$$w = -(6.014 \text{ mol})(8.314 \text{ J K}^{-1} \text{ mol}^{-1})(300 \text{ K}) \ln(2.00 \text{ bar}/6.00 \text{ bar})$$

$$w = 16480 \text{ J}$$

$$q = -16480 \text{ J} \quad (= \Delta U - w = q_{\text{rev}})$$

$$\Delta S = \int \frac{1}{T} dq_{\text{rev}} = \frac{1}{T} \int dq_{\text{rev}} = \frac{-16480 \text{ J}}{300 \text{ K}} = -54.9 \frac{\text{J}}{\text{K}}$$

- b) 75.0 L of helium (assumed to be an ideal gas) at 300 K and 2.00 bar is isothermally compressed to 6.00 bar using a constant 6.00 bar external pressure.

- i) Calculate  $q$ ,  $w$ ,  $\Delta U$  and  $\Delta S$ .

from a:

$$\Delta U = 0 \quad \Delta S = -54.9 \frac{\text{J}}{\text{K}}$$

$U, S$  are state functions, so  $\Delta U, \Delta S$  are path-independent

$$w = -\int P_{\text{ext}} dV = -P_{\text{ext}} \int dV = -P_{\text{ext}} \Delta V = -P_f (V_f - V_i)$$

$$w = -P_f \left( \frac{nRT}{P_f} - \frac{nRT}{P_i} \right) = -nRT \left( 1 - \frac{P_f}{P_i} \right) \quad q = -w = -30,000 \text{ J}$$

$$w = -(6.014 \text{ mol})(8.314 \text{ J K}^{-1} \text{ mol}^{-1})(300 \text{ K}) \left( 1 - \frac{6.00}{2.00} \right) = 30,000 \text{ J}$$

- ii) Use the values of  $q$  and  $\Delta S$  (not your equation sheets!) to prove this compression is irreversible.

$$\int \frac{1}{T} dq = \frac{1}{T} \int dq = \frac{q}{T} = \frac{-30,000 \text{ J}}{300 \text{ K}} = -100.0 \frac{\text{J}}{\text{K}} \neq \Delta S$$

$$\left( \begin{aligned} \text{also: } \Delta S_{\text{sys}} + \Delta S_{\text{sur}} \\ = -54.9 \frac{\text{J}}{\text{K}} + \frac{30,000 \text{ J}}{300 \text{ K}} = +45.1 \frac{\text{J}}{\text{K}} > 0 \end{aligned} \right) \therefore \text{irreversible}$$

for one engine cycle

- Q2. a) The analysis of reversible Carnot engines shows  $\frac{q_C}{T_C} + \frac{q_H}{T_H} = 0$ . How did this result lead to the discovery of the entropy?

suggests  $\int_i^f \frac{dq_{rev}}{T} = 0$   $\frac{dq_{rev}}{T}$  must be the differential of a state function

$$= S_f - S_i$$

- b) A heat engine operating with  $T_C = 300$  K and  $T_H = 500$  K absorbs 100 kJ heat at 500 K and does 20 kJ work on the surroundings. Is the engine operating reversibly? Justify your answer.

reversible-engine efficiency  $\varepsilon = 1 - \frac{T_C}{T_H} = 1 - \frac{300\text{K}}{500\text{K}} = 0.400$

actual engine efficiency  $= \frac{-W}{q_H} = \frac{20\text{ kJ}}{100\text{ kJ}} = 0.200 < \varepsilon$

not reversible  
 $\varepsilon < 1 - \frac{T_C}{T_H}$

- c) What is a heat pump? Why are these devices useful?

- \* a heat engine running in reverse
- \* work is done on the pump to remove heat from the  $T_C$  reservoir and add heat to the  $T_H$  reservoir
- \* used for space heating, refrigeration, air conditioning

- d) The internal energy is conserved in physical and chemical processes:  $\Delta U_{\text{system}} + \Delta U_{\text{surroundings}} = 0$ . Is the entropy conserved in these processes? Explain briefly.

entropy is not conserved

spontaneous processes increase the entropy

$$\left( \Delta S_{\text{sys}} + \Delta S_{\text{sur}} \right)_{\text{spont. process}} > 0$$

- e) Burning hydrogen using pure oxygen produces a flame that is much hotter (by about 1,000 K!) than the flame produced by burning hydrogen in air. Why?

using pure oxygen, the exothermic combustion reaction heats up the  $\text{H}_2\text{O}(g)$  product

using air, the combustion reaction heats up the  $\text{H}_2\text{O}(g)$  product and inert  $\text{N}_2$  (higher heat capacity)  $\rightarrow$  lower temperature reached

Q3. a) Derive the thermodynamic equation of state:  $\left(\frac{\partial U}{\partial V}\right)_T = T\left(\frac{\partial p}{\partial T}\right)_V - p$

Hint: Start with  $dU = TdS - pdV$   $\div dV_T$

$$\left(\frac{\partial U}{\partial V}\right)_T = T\left(\frac{\partial S}{\partial V}\right)_T - p\left(\frac{\partial V}{\partial V}\right)_T = T\left(\frac{\partial p}{\partial T}\right)_V - p$$

from  $dA = -SdT - pdV$  get  $\left(\frac{\partial S}{\partial V}\right)_T = \left(\frac{\partial p}{\partial T}\right)_V$

b) For an ideal gas, prove  $(\partial U/\partial V)_T = 0$ .

$$\left(\frac{\partial U}{\partial V}\right)_T = T\left(\frac{\partial}{\partial T} \frac{nRT}{V}\right)_V - p = T\frac{nR}{V}\left(\frac{\partial T}{\partial T}\right)_V - p = p - p = 0$$

c) For an ideal gas, prove  $\left(\frac{\partial C_V}{\partial V}\right)_T = 0$

Hint:  $C_V = (\partial U/\partial T)_V$

$$\left(\frac{\partial C_V}{\partial V}\right)_T = \left[\frac{\partial}{\partial V} \left(\frac{\partial U}{\partial T}\right)_V\right]_T = \left[\frac{\partial}{\partial T} \left(\frac{\partial U}{\partial V}\right)_T\right]_V = 0$$

d) For an ideal gas undergoing a reversible process, rearranging the First Law ( $dU = C_V dT = dq_{\text{rev}} - pdV$ ) gives

$$\frac{dq_{\text{rev}}}{T} = \frac{C_V}{T} dT + \frac{p}{T} dp \quad (\text{A})$$

Use equation (A) and the test for an exact differential to prove  $dq_{\text{rev}}/T$  is the differential of a state function. Name the state function.

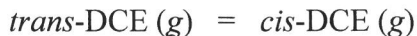
$$\left(\frac{\partial \frac{C_V}{T}}{\partial p}\right)_T = \frac{1}{T} \left(\frac{\partial C_V}{\partial V}\right)_T = 0$$

$$\left(\frac{\partial \frac{p}{T}}{\partial T}\right)_V = \left(\frac{\partial \frac{nRT/V}{T}}{\partial T}\right)_V = \left(\frac{\partial \frac{nR}{V}}{\partial T}\right)_V = 0$$

$\therefore \frac{dq_{\text{rev}}}{T}$  is exact  
 $= dS$   
 $S$  is the entropy

constant at constant  $V$

Q4. This question refers to the isomerization of 1,2-dichloroethylene (DCE) at 25 °C.



Data at 25 °C:  $\Delta H_{\text{fm}}^\circ(\text{trans-DCE, g}) = 6.15 \text{ kJ mol}^{-1}$   
 $\Delta H_{\text{fm}}^\circ(\text{cis-DCE, g}) = 3.77 \text{ kJ mol}^{-1}$

$$\Delta G_{\text{m}}^\circ(\text{trans-DCE, g}) = 28.57 \text{ kJ mol}^{-1}$$

$$\Delta G_{\text{m}}^\circ(\text{cis-DCE, g}) = 26.31 \text{ kJ mol}^{-1}$$

- a) 10.0 moles of *trans*-DCE are loaded into a 250.0 L tank at 25 °C. Calculate the number of moles of *trans*-DCE and the number of moles of *cis*-DCE at equilibrium.

$$\Delta G^\circ = \Delta G_{\text{fm}}^\circ(\text{cis}) - \Delta G_{\text{fm}}^\circ(\text{trans}) = 26.31 - 28.57 = -2.26 \text{ kJ}$$

$$K = \frac{P_{\text{cis}}}{P_{\text{trans}}} = e^{-\Delta G^\circ/RT} = e^{-(-2260\text{J})/(8.314\text{ J K}^{-1}\text{ mol}^{-1})298.15\text{K}}$$

$$K = e^{0.9117} = 2.489 = \frac{\frac{n_{\text{cis}}RT}{V}}{\frac{n_{\text{trans}}RT}{V}} = \frac{n_{\text{cis}}}{n_{\text{trans}}}$$

$$K = \frac{x}{10.0 \text{ mol} - x} = 2.489 \quad x = 7.13 \text{ mol}$$

$$n_{\text{trans}} = (10.00 - 7.13) \text{ mol} = \boxed{2.87 \text{ mol}}$$

$$\boxed{n_{\text{cis}} = 7.13 \text{ mol}}$$

- b) The Gibbs energy of formation of *cis*-DCE is lower than that of *trans*-DCE, indicating *trans*-DCE is unstable relative to *cis*-DCE. Why doesn't the unstable *trans*-DCE convert completely to *cis*-DCE?

back reaction of the pure *cis* isomer to produce the *trans* isomer produces a lower Gibbs energy due to  $\Delta G_{\text{mix}}$

- c) For a higher yield of the *cis*-DCE product, should the temperature be increased? Justify your answer.

$$\Delta H^\circ = \Delta H_{\text{fm}}^\circ(\text{cis}) - \Delta H_{\text{fm}}^\circ(\text{trans})$$

$$= (3.77 - 6.15) \text{ kJ}$$

$$= -2.38 \text{ kJ (exothermic)}$$

$$\frac{d \ln K}{dT} = \frac{\Delta H^\circ}{RT^2} < 0$$

lower T to get more *cis* isomer

- d) For a higher yield of *cis*-DCE, should the pressure in the tank be increased? Justify your answer.

pressure had no effect on the yield of the *cis* isomer

$$(\Delta n_{\text{gas}} = 0)$$